ION-EXCHANGE SEPARATION OF SODIUM AND POTASSIUM WITH COUNTER-CURRENT OF ELUENT AND ELECTROMIGRATION

Yoshihiro MORI. Tetsuo OOYASU, and Hiroyuki MATSUDA Department of Chemistry, Faculty of Science, Shinshu University 3-1-1 Asahi, Matsumoto, Nagano 390

The translation of Na with an eluent on strong electrolyte cation exchanger column is larger than that of K+, but with electromigration smaller than that of K+. An effective separation of Na+ and K+ may be expected with a simultaneous use of ion-exchange and electromigration. When an electric field[150 v(between electrodes), 3.3 mA] was applied on a strong electrolyte cation exchanger(Diaion PK-228) column(height; 10 cm, diameter; 1 cm) with parallel but reverse direction to the eluent(0.1 N NH,Cl) flow, Na and K(each 0.5 meq) have been separated perfectly by the elution.

The simultaneous use of ion-exchange and electromigration in the vertical and the horizontal directions, respectively, has been reported already for continuous isotope enrichment. Now, the separations of sodium and potassium were attempted by a simultaneous use of ion-exchange and electromigration in vertical but reverse directions. It is well known that the potassium affinities for a strong electrolyte cation exchanger

from relatively dilute aqueous solutions are higher than the sodium affinities. In consequence, the translation of sodium on the ion-exchange column by eluents is generally larger than that of potassium. The electromigration velocity of potassium is larger than that of sodium in aqueous solutions³⁾as well as in the strong electrolyte cation exchange resin. When the direction of electromigration is opposite to the flow of eluent, the differences in the translation velocities of Na and K on the ion-exchange column are larger than the differences by eluent only, and the separation of $\ensuremath{\mathsf{K}}$ and Na will be attained effectively.

An ion exchange column(height; 10 cm, diameter; 1 cm) was made with Diaion PK-228 NH $_{\Lambda}$ -form(100 \sim 150 mesh) (Fig. 1). On the top of the column, 0.5 meq. Na and 0.5 meq. K ions were absorbed from a mixed solution and the column was washed with deionized water. The electric field was not applied in the first experiment with the eluent of 0.1 N NH, Cl solution(flow rate; 1.2 ml/min) and in the second experiment the electric field[150 v

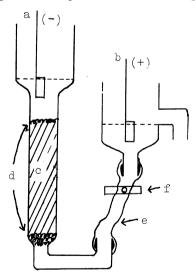


Fig.1 Ion exchange column with electromigration

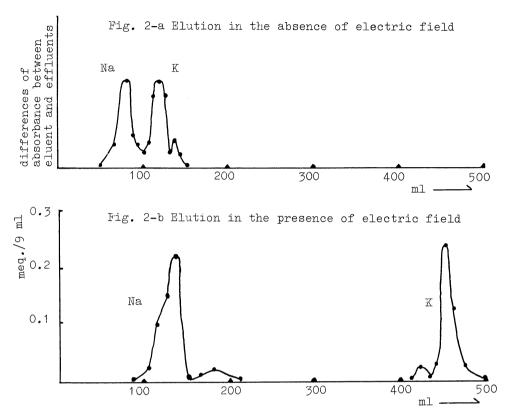
a, b; platinum electrode

c; ion-exchanger

d; glass wool e; flexible tube

f; screw cock

(between electrodes), 3.3 mA] was applied. The effluents were collected with a fraction collector, and the concentration of NH_4 on each fration was determined by a spectrophotometric method. The differences of the NH_4 concentrations between the eluent and the effluents were considered to be alkali concentration in the effluents. The elution curves of Na and K ions are shown in Figs. 2-a and -b.



Sodium and potassium in the effluent were estimated by flame tests and by the measurements of weight and equivalents of the chlorides after eliminating NH₄ with OH-form strong electrolyte anion exchanger. In Fig. 2-a, the distance between the peaks of Na and K is 35 ml in the elution volume, and overlapping of the elution curves is observed. When the electric field was applied(in Fig. 2-b), the corresponding distance is 297 ml, and the two elution curves are completely separated from each other. The separation of Na and K proceed perfectly with a relatively short ion-exchange column. Na and K in effluent were found to be 0.47 meq. and 0.50 meq. respectively.

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